



Understanding Combustion Processes Through Microgravity Research

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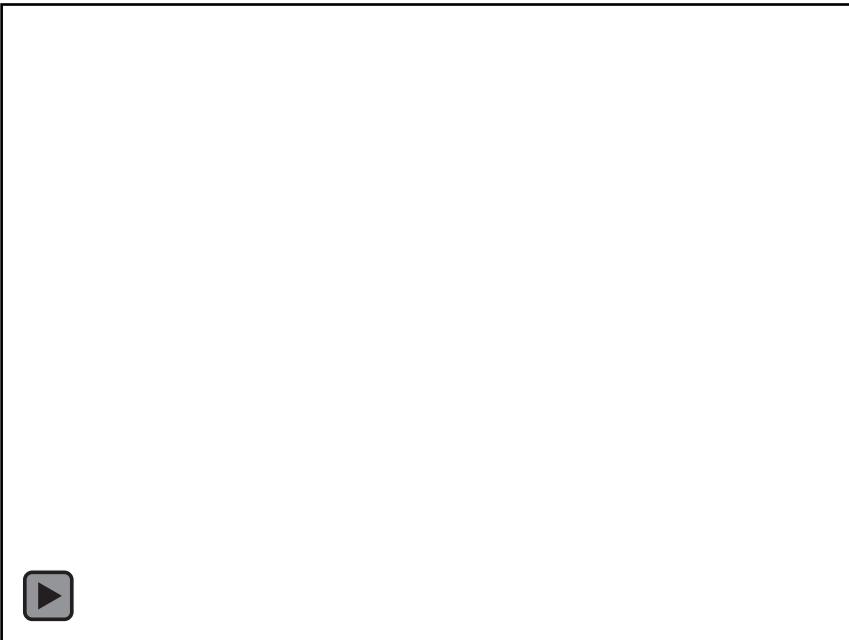
- Gravity influences combustion through
 - Buoyant convection
 - Deformation / dropping of liquid droplets
 - Sedimentation in multi-phase systems
- Eliminating gravity enables observation of processes overwhelmed by gravity on earth
- Applications
 - Spacecraft fire safety
 - Better understanding of combustion at earth gravity

- Chemical time (t_{chem}) $\approx \delta/S_L \approx (\alpha/S_L)/S_L \approx \alpha/S_L^2$
 α = thermal diffusivity
 S_L = laminar flame speed ≈ 40 cm/s for stoichiometric hydrocarbon-air; ≈ 5 for near-limit mixtures
- Buoyant transport time $\approx d/U$; $U \approx (gd(\Delta\rho/\rho))^{1/2} \approx (gd)^{1/2}$
(g = gravity, d = characteristic dimension)
 - Inviscid: $t_{\text{inv}} \approx d/(gd)^{1/2} \approx (d/g)^{1/2}$
 - Viscous: $d \approx \nu/U \Rightarrow t_{\text{vis}} \approx (\nu/g^2)^{1/3}$ (ν = viscosity)
- Conduction time (t_{cond}) $\approx T_f/(dT/dt) \approx d^2/16\alpha$
- **Radiation time** (t_{rad}) $\approx T_f/(dT/dt) \approx T_f/(\Lambda/\rho C_p)$
 - Optically thin: $\Lambda = 4\sigma a_p (T_f^4 - T_\infty^4)$ (radiative loss rate / volume)
(a_p = Planck mean absorption coefficient)
 $\Rightarrow t_{\text{rad}} \sim P/\sigma a_p (T_f^4 - T_\infty^4) \sim P^0$, P = pressure

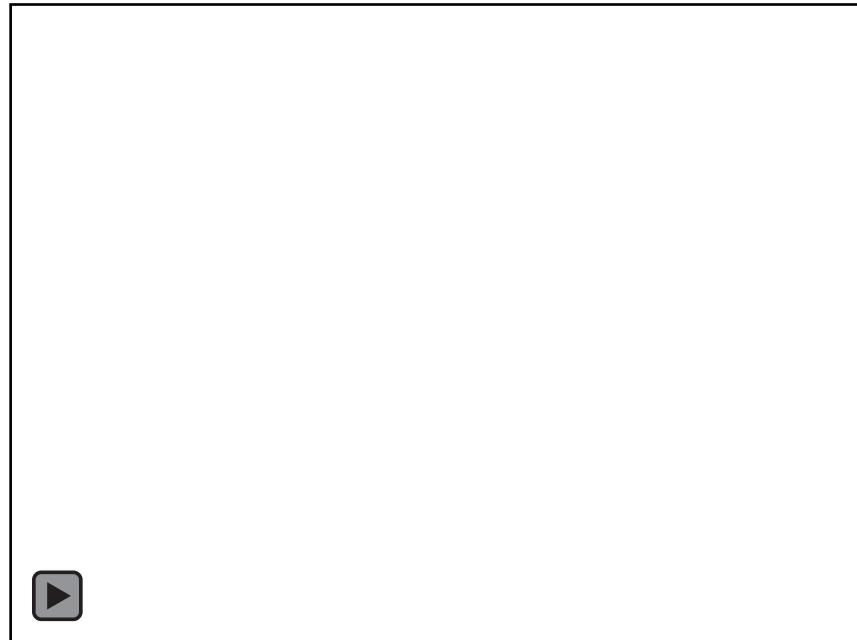
Time scale	Stoich. flame	Limit flame
Chemistry (t_{chem}) or diffusion (t_{diff})	0.00094 s	0.25 s
Buoyant, inviscid (t_{inv})	0.071 s	0.071 s
Buoyant, viscous (t_{vis})	0.012 s	0.010 s
Conduction (t_{cond}), $d = 5 \text{ cm}$	0.95 s	1.4 s
Radiation (t_{rad})	0.13 s	0.41 s

- Conclusions
 - Buoyancy unimportant for near-stoichiometric flames
($t_{\text{inv}} \& t_{\text{vis}} \gg t_{\text{chem}}$)
 - Buoyancy strongly influences near-limit flames at 1g
($t_{\text{inv}} \& t_{\text{vis}} < t_{\text{chem}}$)
 - Radiation effects unimportant at 1g ($t_{\text{vis}} \ll t_{\text{rad}}; t_{\text{inv}} \ll t_{\text{rad}}$)
 - Radiation effects dominate flames with low S_L ($t_{\text{rad}} \approx t_{\text{chem}}$), but only observable at μg
 - Radiation $>$ conduction only for $d > 3 \text{ cm}$
 - Radiation time scale t_{rad} is small enough ($\approx 1 \text{ s}$) that radiation effects on flames can be observed in drop tower experiments
 - Reynolds number $\sim Vd/\nu \sim (gd^3/\nu^2)^{1/2} \Rightarrow$ turbulent flow unavoidable at 1g for large systems ($d > 10 \text{ cm}$)

- Limit composition, propagation speed, and shape depend on orientation - *buoyancy effects*



Upward propagation



Downward propagation

- Big tube, no gravity – extinction caused by radiative loss

$(t_{\text{chem}} \approx t_{\text{rad}})$

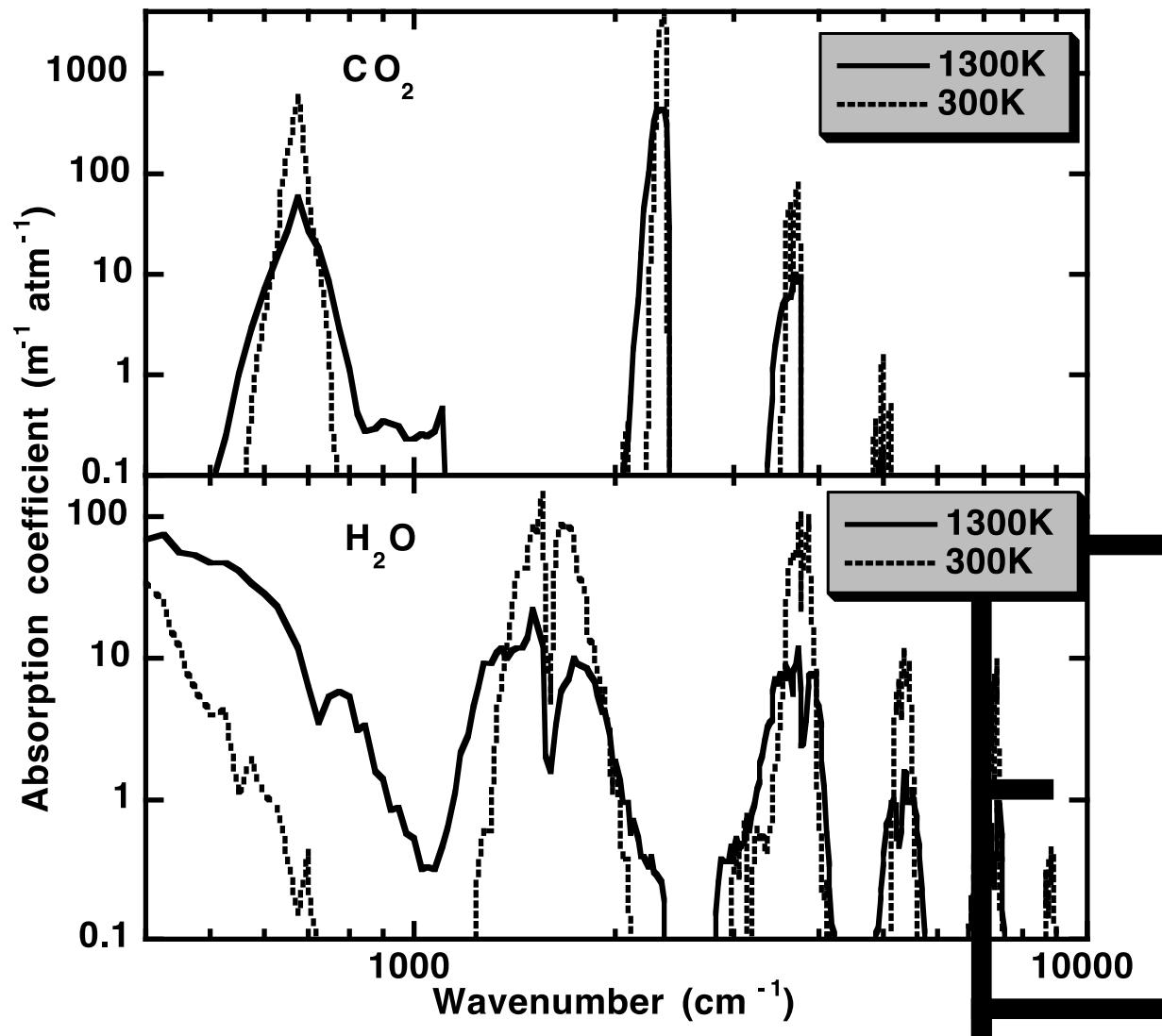
$$S_{L,\text{lim}} = \frac{1}{\rho_{\infty} C_p} \sqrt{\frac{1.2 \beta \Lambda \lambda_f}{T_f}} \quad (\text{no reabsorption})$$

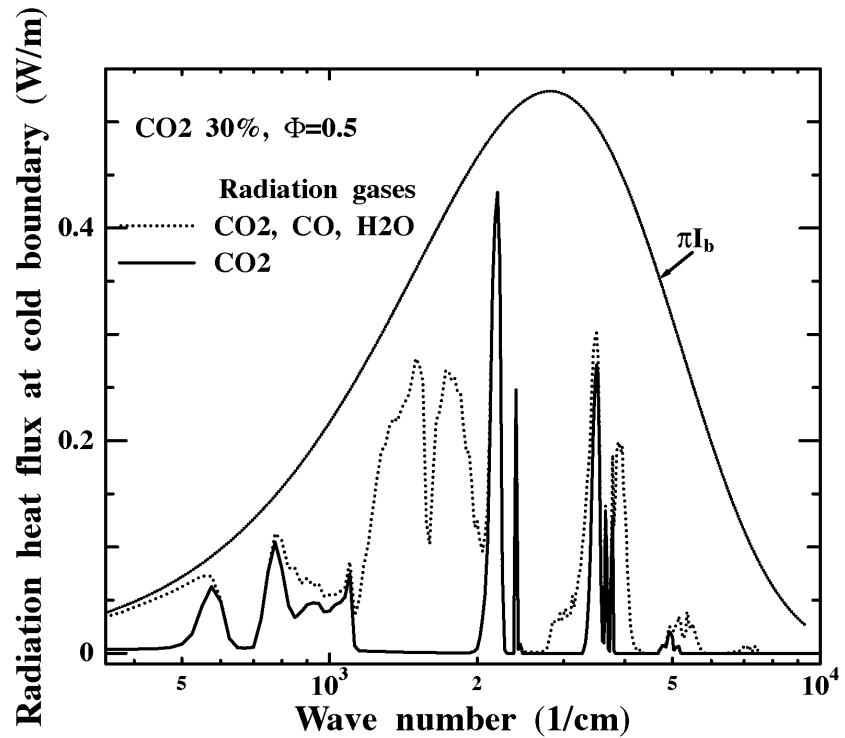
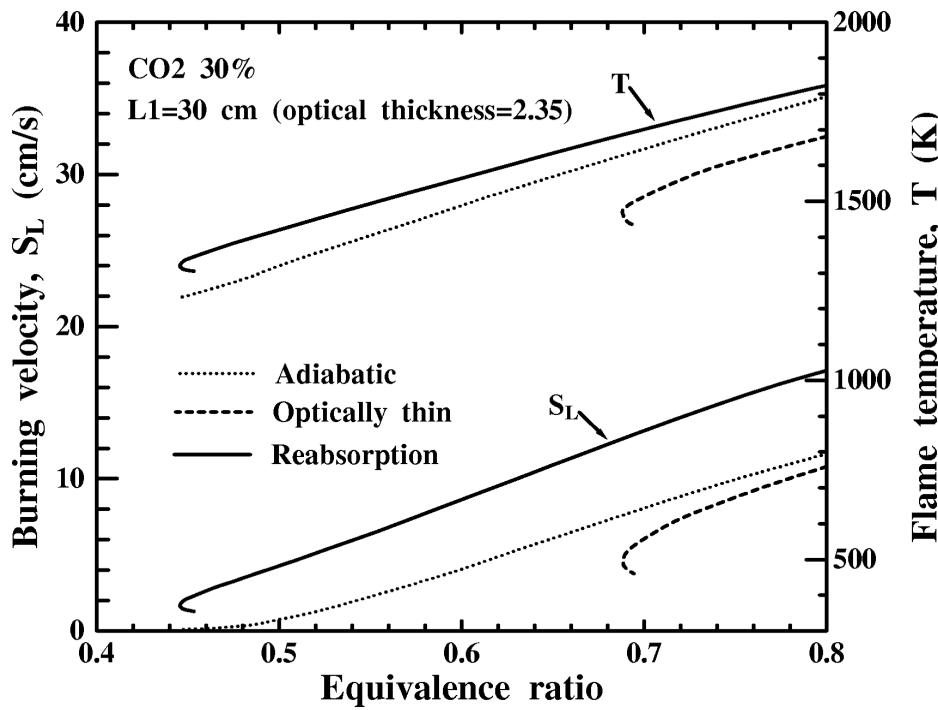
- prediction consistent with μg experiments

$$\text{Impact of heat loss} \sim \frac{\text{Heat loss}}{\text{Heat release}} \sim \frac{T^2}{e^{-E/RT}} \quad \uparrow \text{ as } T \downarrow$$

- **Reabsorption** significant when $a_p^{-1} < d$
 - Extends limits & increases S_L – theoretically no limit with graybody absorbers
 - Gases – spectral radiation – 2 mechanisms allow radiation to escape even with reabsorption
 - » Absorption spectra of products different from reactants
 - » Spectra broader at high T than low T

Absorption spectra of H_2O & CO_2





Methane-air mixtures with 30% of N_2 replaced with CO_2 , 1 atm

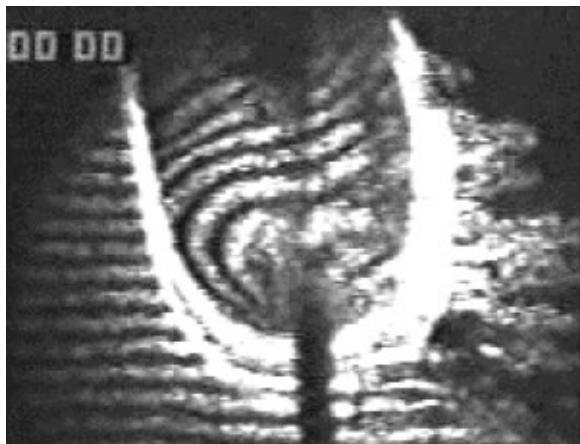
- Flame spread rate (S_f) with opposing flow U , infinite-rate kinetics (mixing limited)

$$S_f = \frac{\pi}{4} \frac{\lambda_g}{\rho_s C_{p,s} \tau_s} \frac{T_f - T_v}{T_v - T_\infty} \quad (\text{thin fuel}) - \text{independent of } P \text{ and } U$$

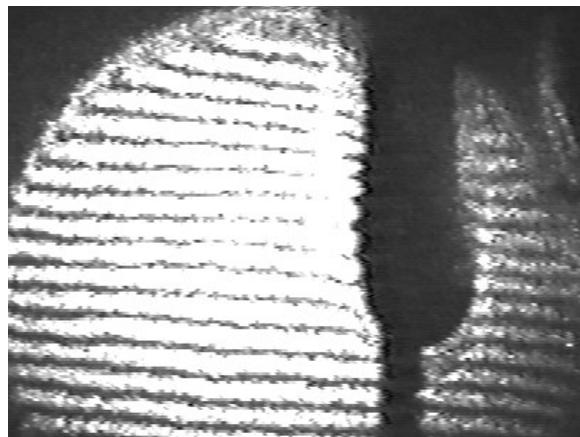
$$S_f = U \frac{\lambda \rho C_p}{\lambda_s \rho_s C_{p,s}} \left(\frac{T_f - T_v}{T_v - T_\infty} \right)^2 \quad (\text{thick fuel}) - S_f \sim P^1 U^1$$

- Diffusive transport time scale (t_{diff}) $\approx \delta/U \approx \alpha/U^2$
- Heat loss parameter $H \sim t_{\text{diff}}/t_{\text{rad}} = \alpha/U^2 t_{\text{rad}} \sim P^{-1} U^{-2}$
 - Optically-thin: S_f lower at μg : $U = S_f \ll U(1g) \Rightarrow$ higher H
 - Dual-limit behavior
 - » Large U : residence-time limited: $t_{\text{diff}} \leq t_{\text{chem}}$
 - » Small U : heat loss: $t_{\text{diff}} \geq t_{\text{rad}}$
 - » Most robust $U \approx 10 \text{ cm/s}$ - less than 1g buoyant flow!
- Radiation not all lost if ambient atmosphere absorbs
 - O_2-N_2 , O_2-He , O_2-Ar : $S_f(1g) > S_f(\mu g)$ due to radiative loss
 - O_2-CO_2 , O_2-SF_6 : $S_f(1g) < S_f(\mu g)$ due to reabsorption
 - International Space Station uses CO_2 fire extinguishers!

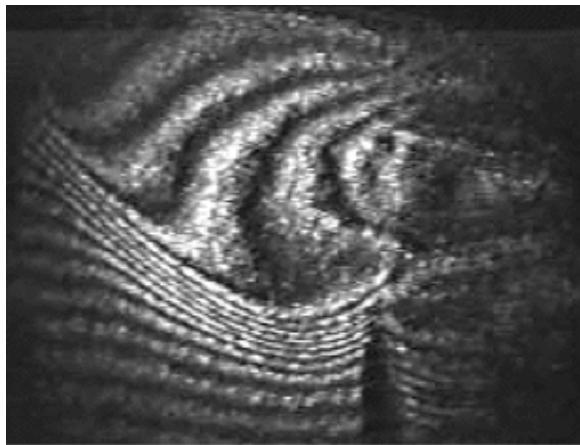
Flame spread - 1g vs. μ g, optically-thin vs. thick



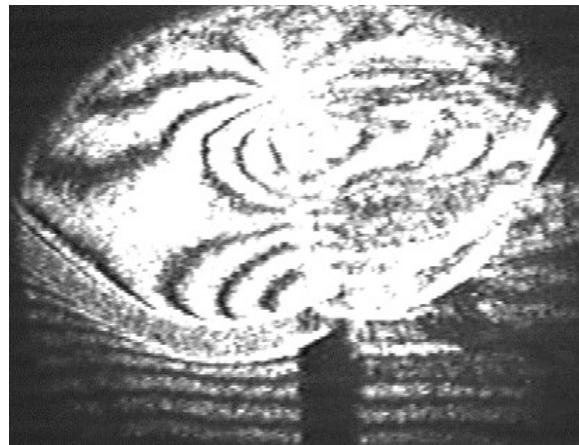
30% O₂ in N₂, 1g



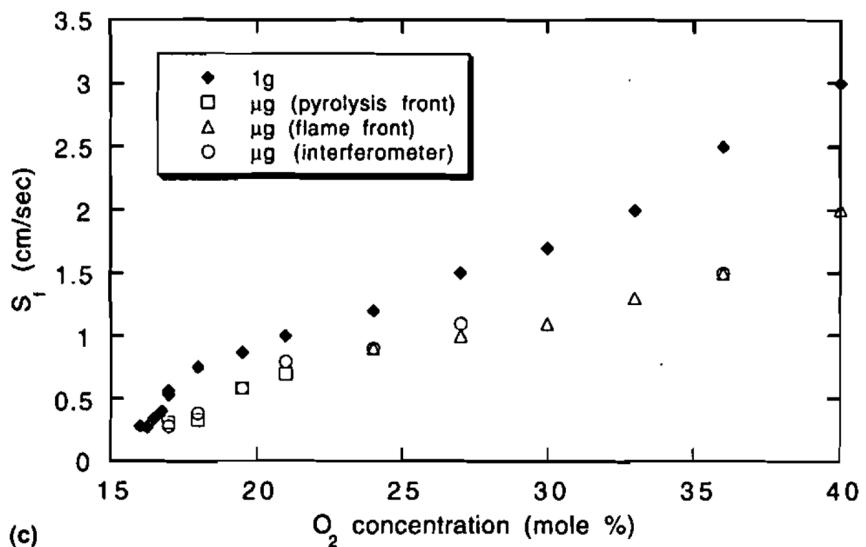
42% O₂ in SF₆, 1g



30% O₂ in N₂, μ g

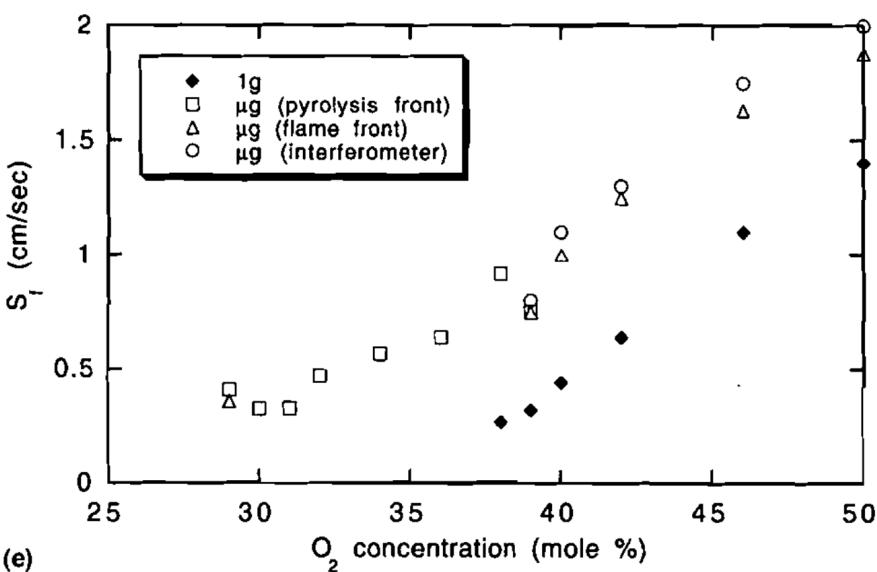


42% O₂ in SF₆, μ g



(c)

N_2 inert



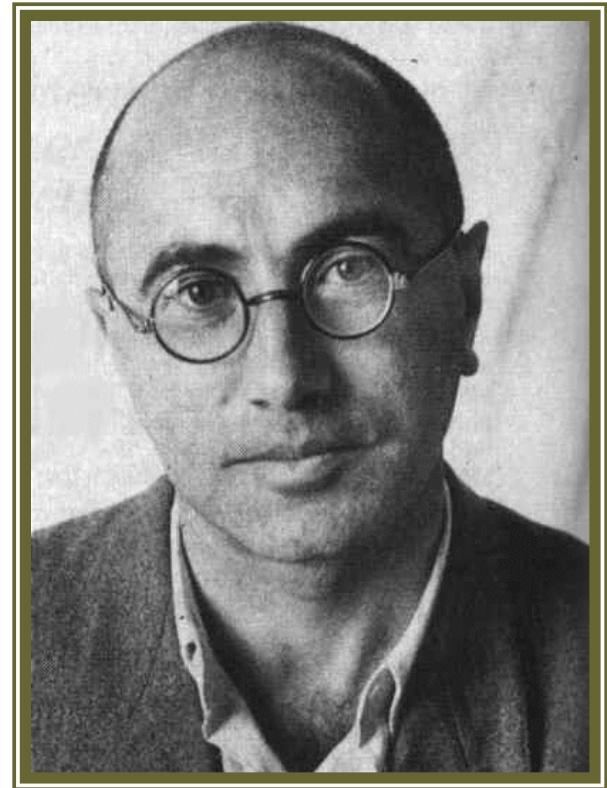
(e)

SF_6 inert

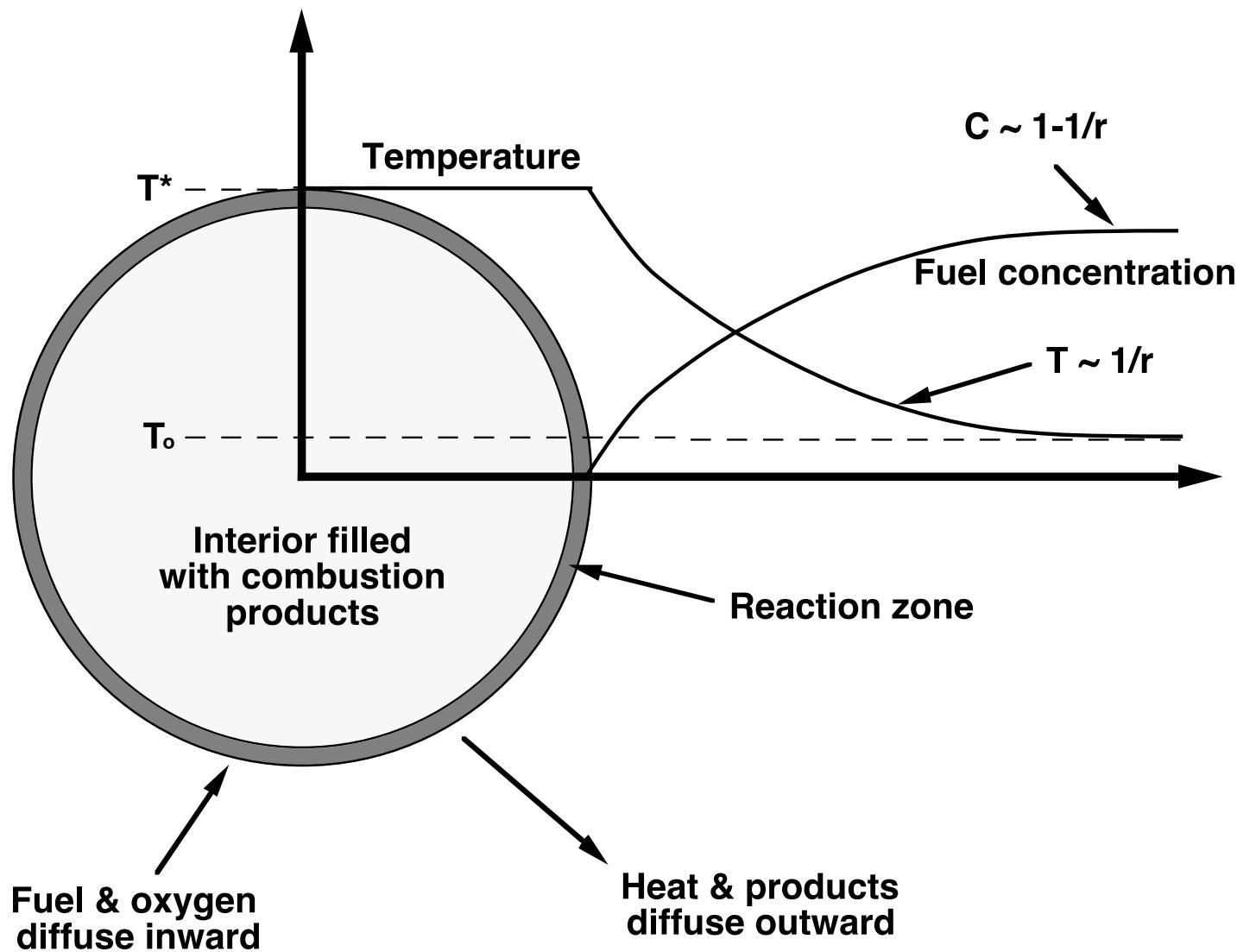
- What we have learned from μ g combustion research?
 - Time scales
 - » *when buoyancy, radiation, etc. is important*
 - Radiative loss – gas-phase & soot
 - » *causes many of the observed effects on burning rates & extinction conditions*
 - Dual limits (high-speed blow-off & low-speed radiative)
 - » *seen for practically all types of flames studied to date*
 - Spherical flames (flame balls, droplets, \approx candle flames)
 - » *long time scales, large domains of influence, radiative loss*
 - Oscillations near extinction
 - » *Common, not yet fully understood*
 - Thermophoresis in sooting flames
 - » *Affects net heat release, soot oxidation, radiative loss*
- Challenges
 - Reabsorption of emitted radiation – scale and spectrum-dependent
 - Chemistry of near-limit mixtures
 - Soot formation, accumulation, oxidation, radiation

BACKUP SLIDES

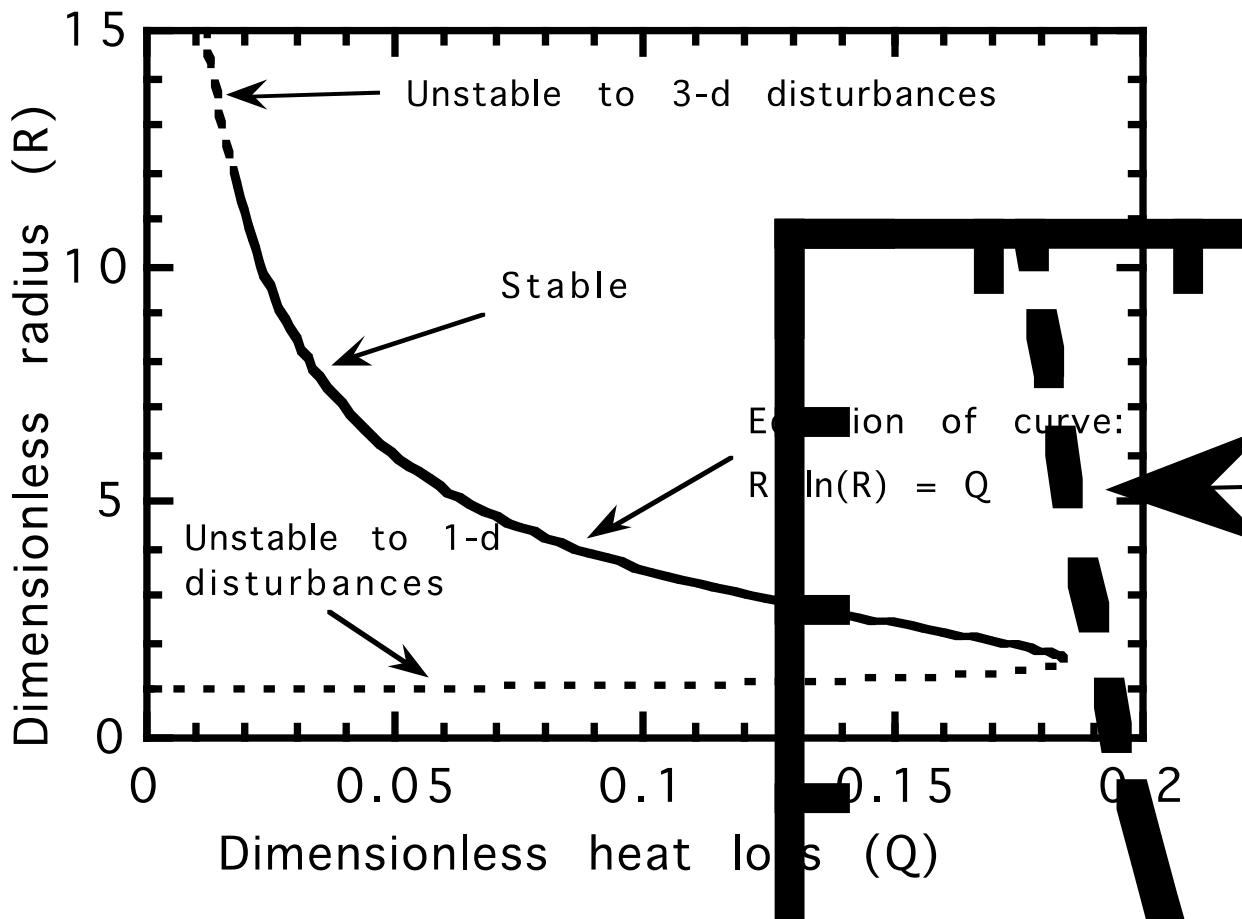
- Zeldovich, 1944: stationary spherical flames possible since $\nabla^2 T$ & $\nabla^2 C = 0$ have solutions for *unbounded* domain in spherical geometry
- Mass conservation requires $U \equiv 0$ everywhere (no stretch) – only diffusive transport
- $T \sim 1/r$ - unlike propagating flame where $T \sim e^{-r}$ - dominated by $1/r$ tail (with r^3 volume effects!)
- Buckmaster, 1985; Joulin, 1985: adiabatic flame balls are *unstable*



Flame ball schematic

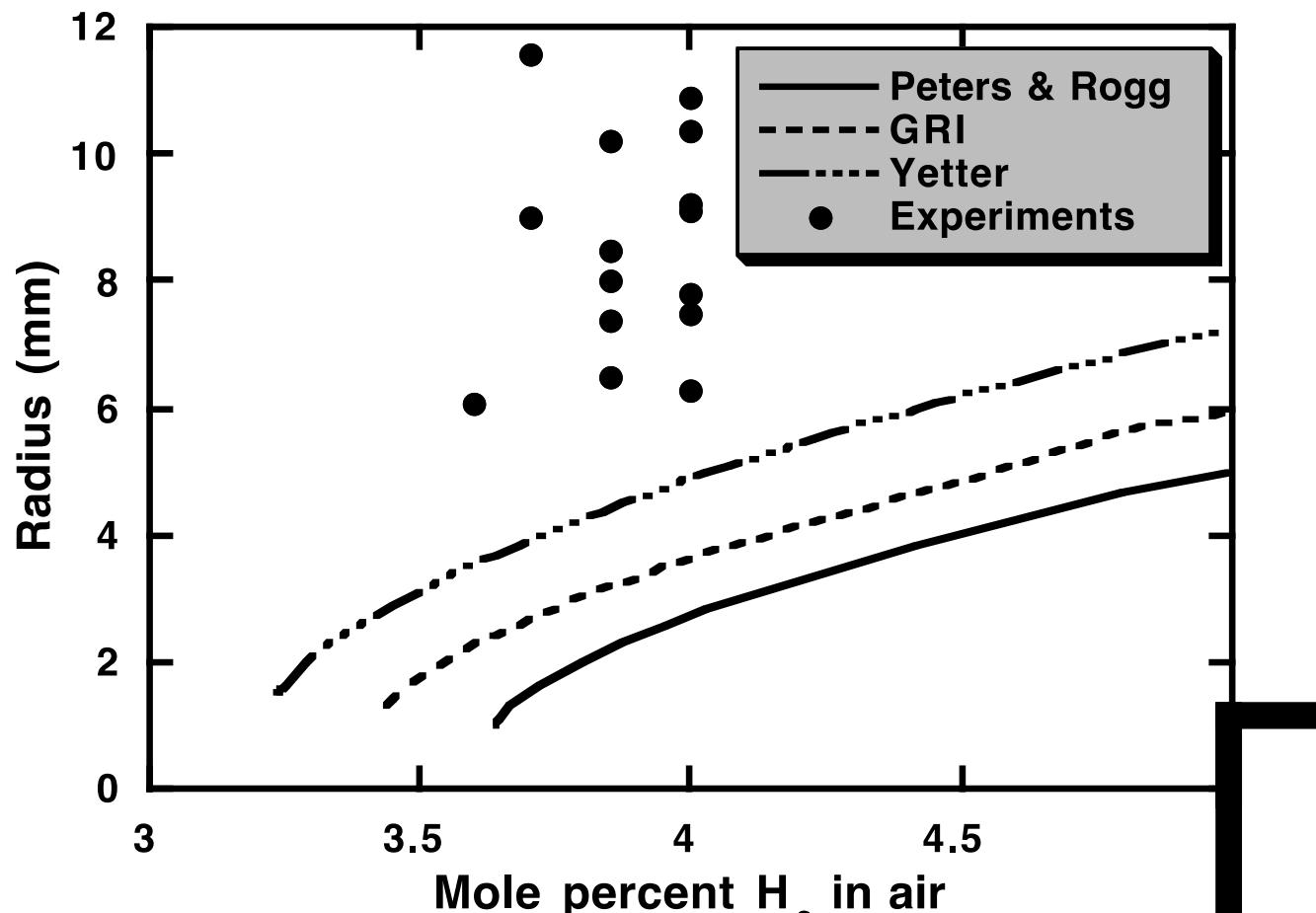


- Ronney (1990): seemingly stable, stationary flame balls accidentally discovered in drop-tower experiment
- Confirmed in parabolic aircraft flights (Ronney *et al.*, 1993)
- Only seen at μg , low Le , near extinction limits
- Space experiments (STS-83 & 94, 1997)
 - Stable for > 500 seconds (!)
 - Weakest flames ever burned (1 – 2 Watts/ball)
 - Very long evolution time scales $\sim (\beta r^*)^2/\alpha \approx 100$ s
- Buckmaster, Joulin & collaborators: window of *stable* conditions with radiative loss & low Le
- Detailed numerical modeling (Yale, USC)
 - Dual limits
 - Unsatisfactory agreement with experiment
 - Results sensitive to $H + O_2 + H_2O \rightarrow HO_2 + H_2O$
 - Reabsorption effects in $H_2-O_2-CO_2$ & $H_2-O_2-SF_6$ mixtures
 - ???

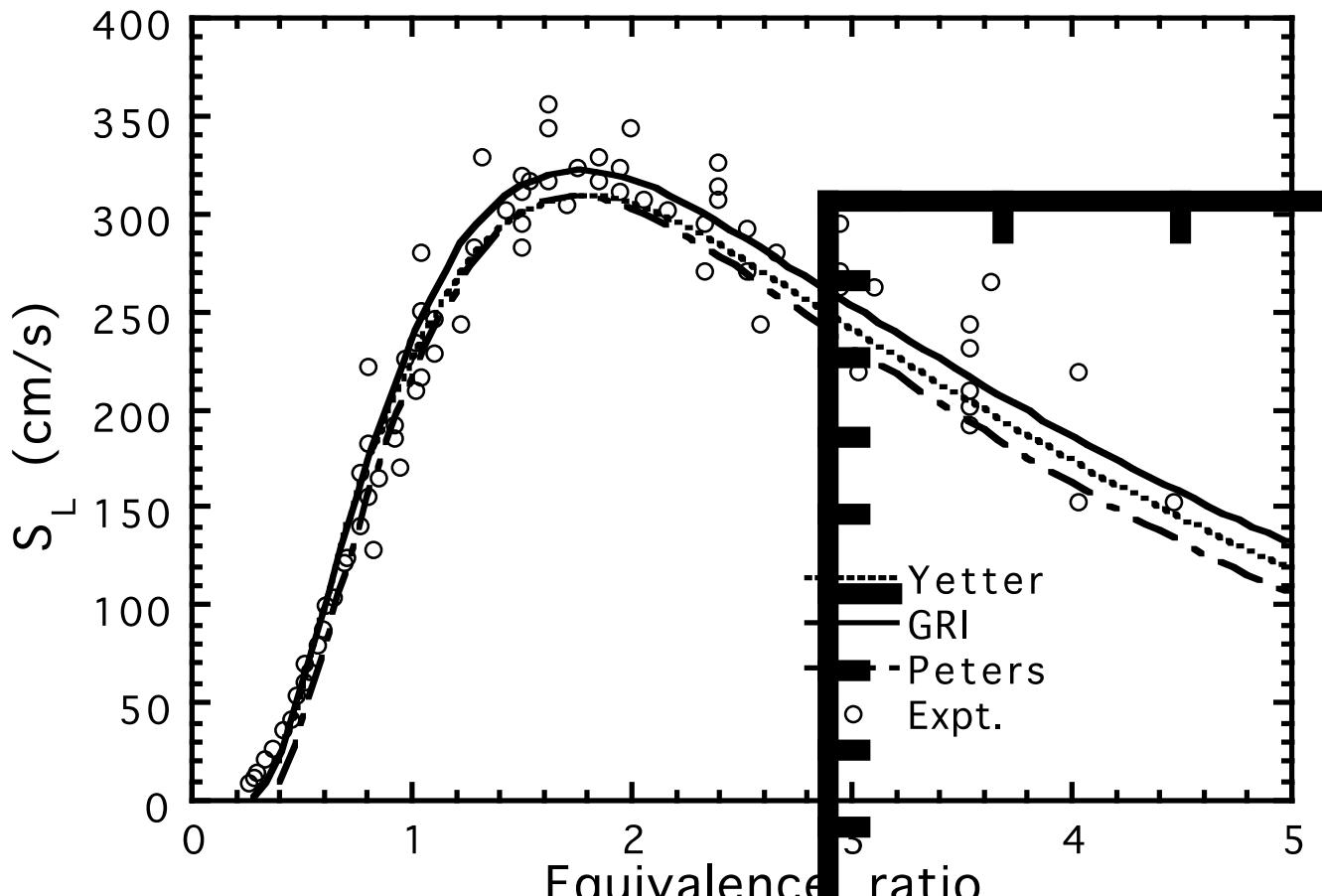


Buckmaster, Joulin, Ronney (1990)

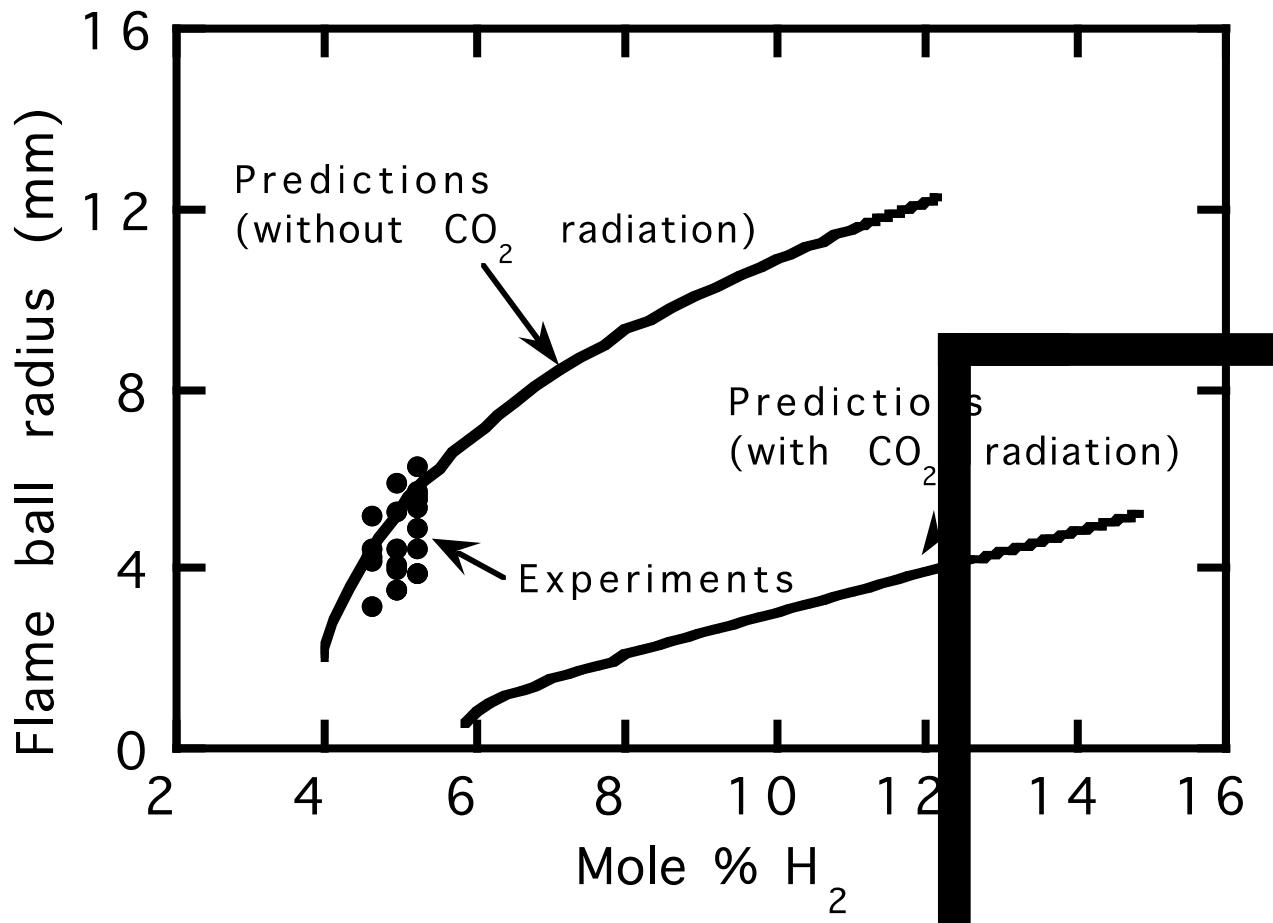
Comparison of predicted & measured radii



H_2 -air mixtures, 1 atm



H_2 -air mixtures, 1 atm



$\text{H}_2\text{-O}_2\text{-CO}_2$ mixtures ($\text{H}_2\text{:O}_2 = 1:2$)

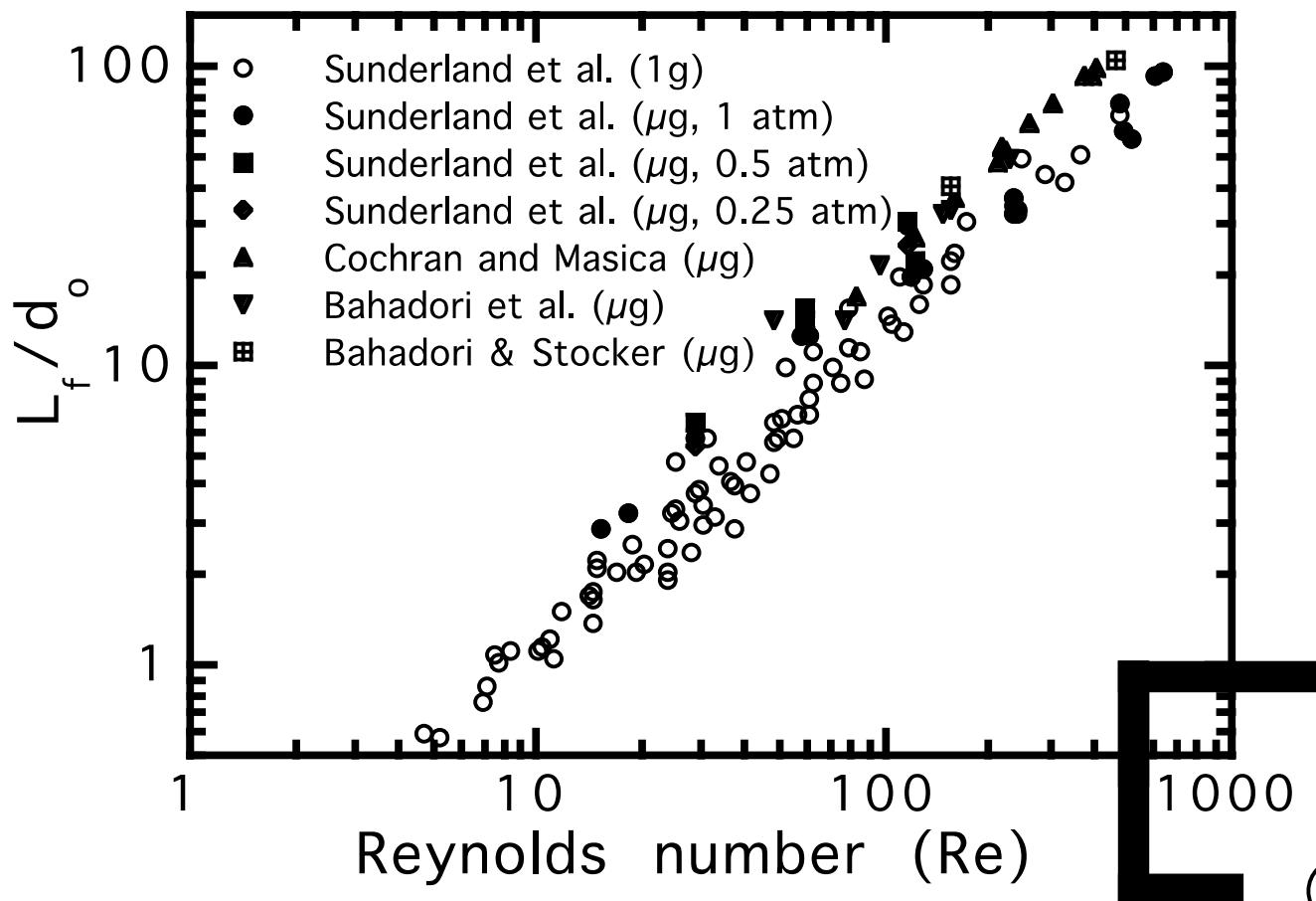
- Counterflow flames
 - Nonpremixed flames – less freedom of movement – flame must lie where stoichiometric flux ratio maintained
 - Radiating gas volume \sim flame thickness $\sim (\alpha/\Sigma)^{1/2}$
- Computations & μg experiments – simple C-shaped dual-limit response
- Conductive loss to burners at low Σ ? $(\Sigma_{\min})^{-1} \approx t_{\text{cond}}$

- Flame height (L_f) and residence time (t_{jet}) determined by equating diffusion time (d^2/D) to convection time (L_f/U)
- Mass conservation: $U(0)d(0)^2 \sim U(L_f)d(L_f)^2$ (round jet); $U(0)d(0) \sim U(L_f)d(L_f)$ (slot jet)
- Buoyant flow: $U(L_f) \sim (gL_f)^{1/2}$; nonbuoyant: $U(L_f) = U(0)$

Geometry	Flow	L_f	t_{jet}
Round-jet	Momentum	$U_o d_o^2 / D$	d_o^2 / D
Round-jet	Buoyant	$U_o d_o^2 / D$	$(U_o d_o^2 / gD)^{1/2}$
Slot-jet	Momentum	$U_o d_o^2 / D$	d_o^2 / D
Slot-jet	Buoyant	$(U_o^4 d_o^4 / D^2 g)^{1/3}$	$(U_o^2 d_o^2 / g^2 D)^{1/3}$

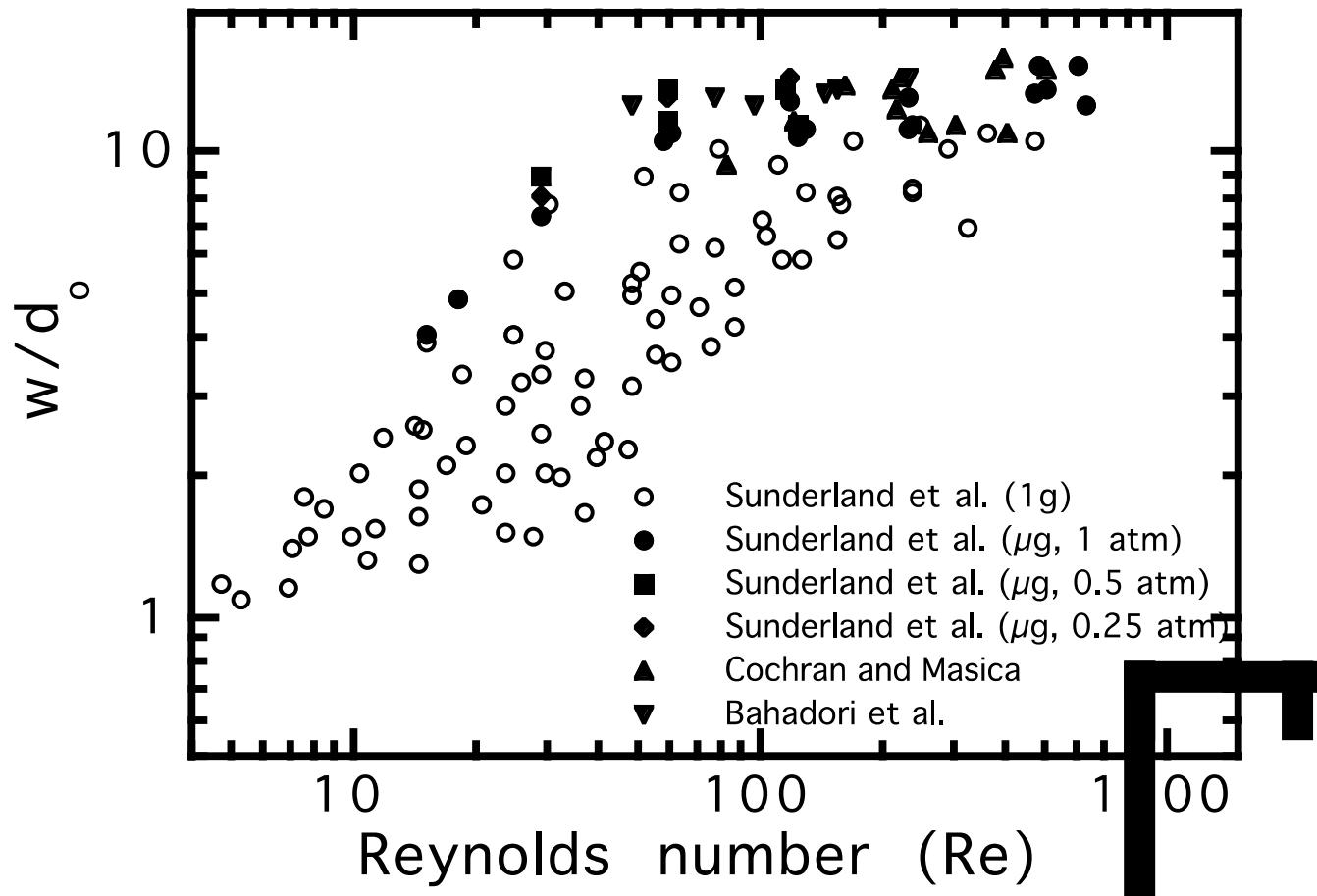
- $L_f \approx$ same at 1g or μg for round jet (what about slot jet?)
- t_{jet} larger at μg than 1g for round jet
 - ⇒ Larger μg flame width $\sim (Dt_{jet})^{1/2}$ - greater difference at low Re due to axial diffusion & buoyancy effects
 - ⇒ Greater radiative loss fraction at μg ($\approx 50\%$ vs. 8%)
- Turbulent flames: $D \sim u'L_I$; $u' \sim U_o$; $L_I \sim d_o$
 - ⇒ $L_f \sim d_o$ (independent of Re)
 - Differences between 1g & μg seen even at high Re - buoyancy effects depend on entire plume
- Soot formation
 - Typically greater at μg due to larger t_{jet} - outweighs lower T
 - Smoke points seen at μg - WHY???
 - » $t_{jet} \sim U_o^{1/2}$ for buoyant flames BUT...
 - » t_{jet} independent of U_o for nonbuoyant flames !
 - » Axial diffusion effects negligible at $Re > 50$
 - Thermophoresis effects - concentrates soot in annulus

Flame lengths at 1g and μ g

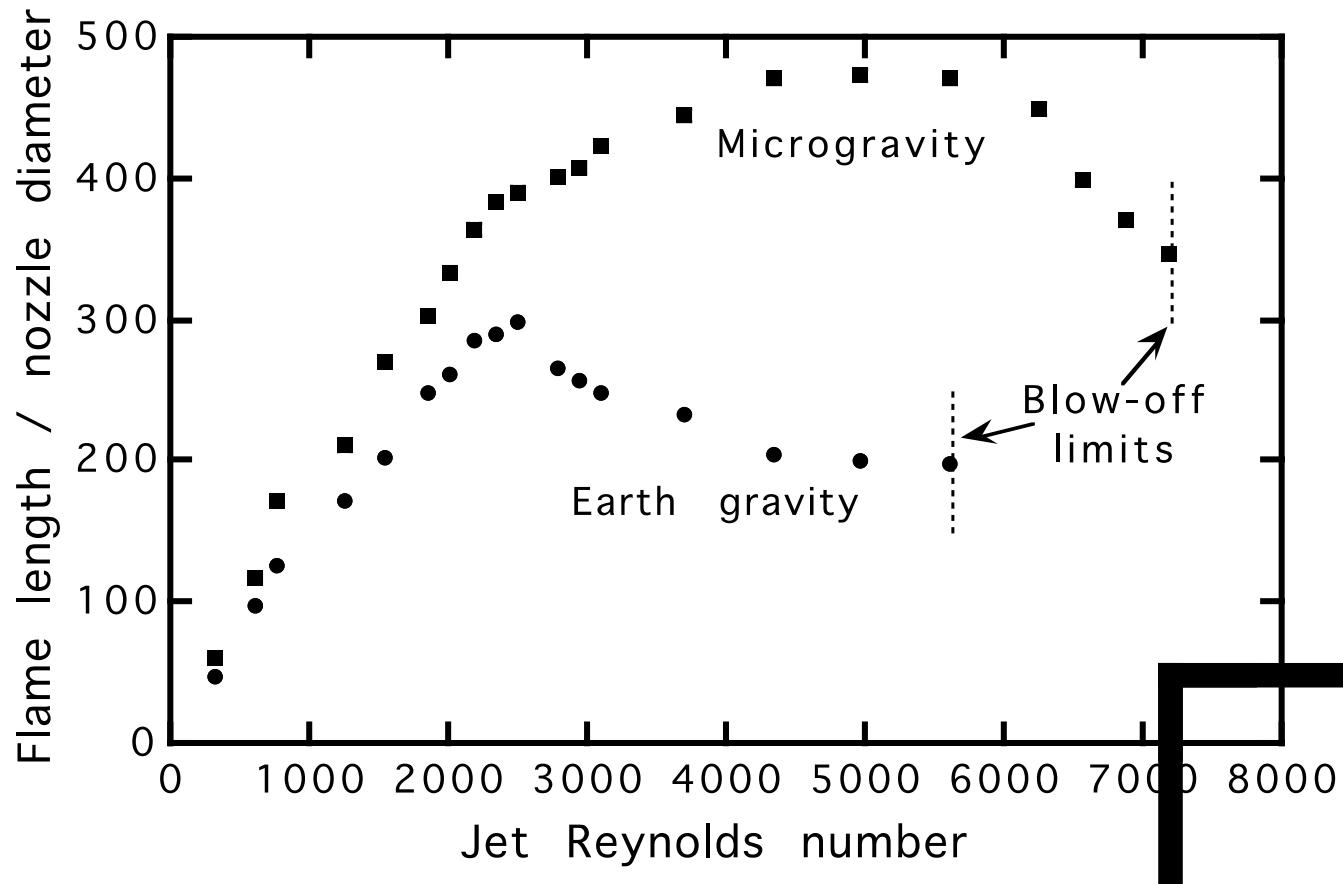


Sunderland et al. (1998) - CH_4/air

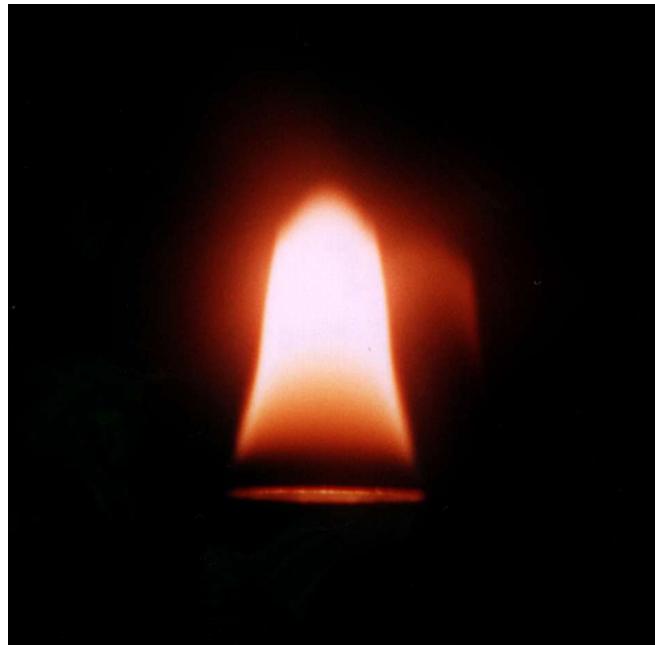
Flame widths at 1g and μ g



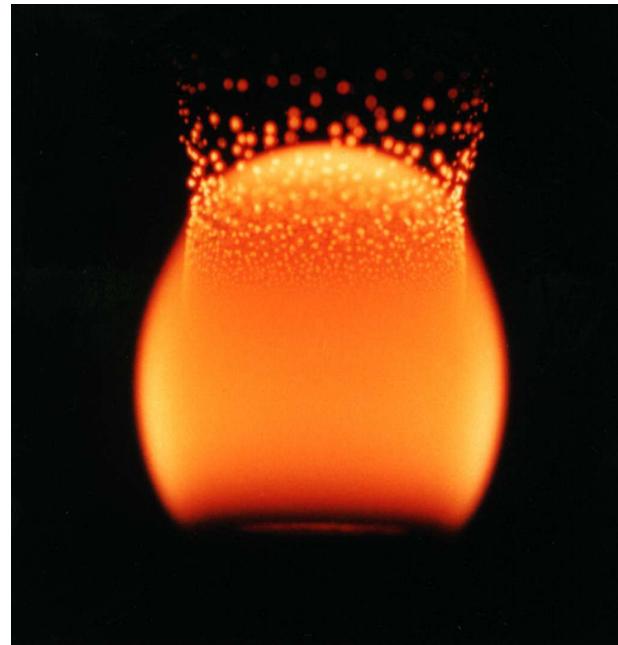
Sunderland et al. (1998) - CH_4/air



Bahadori *et al.* (1997) - $\text{C}_3\text{H}_8/\text{air}$



1g



μ g

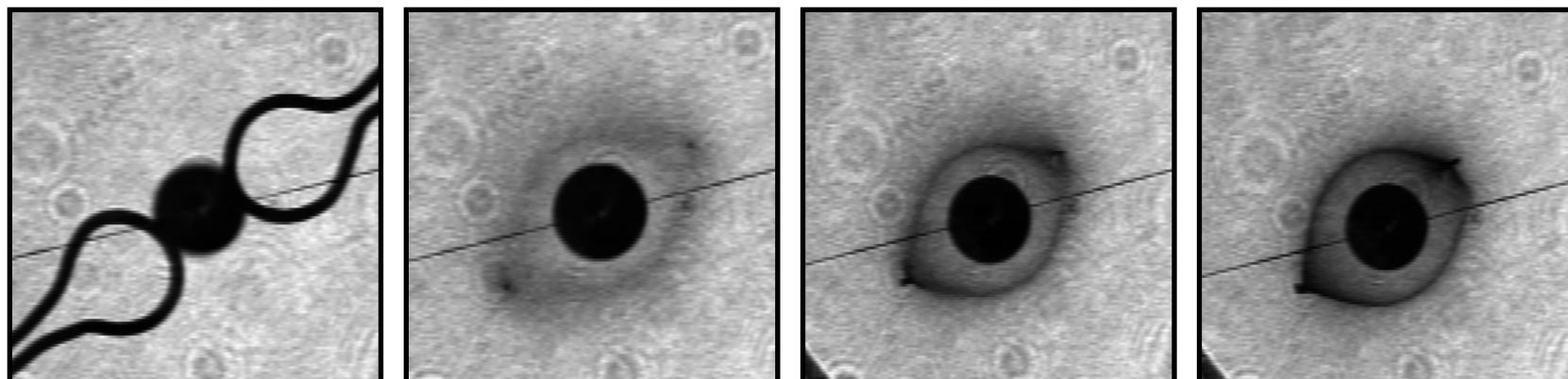
n-butane in air, 10mm diameter jet, $Re = 42$

Fujita *et al.*, 1997

- Spherically-symmetric model (Godsave, Spalding 1953)
 - Steady burning possible - similar to flame balls
(large radii: transport diffusion-dominated)
 - Mass burning rate = $(\pi/4)\rho_d d_d K$; $K = (8\lambda/\rho_d C_P) \ln(1+B)$
 - Flame diameter $d_f = d_d \ln(1+B) / \ln(1+f)$
 - Regressing droplet: $d_{do}^2 - d_d(t)^2 = Kt$ if quasi-steady
- 1st μg experiment - Kumagai (1957) - $K(\mu\text{g}) < K(1\text{g})$
- Dual-limit behavior
 - Residence-time limited (small d_d): $t_{drop} = d_f^2/\alpha \leq t_{chem}$
 - Heat loss (large d_d): $t_{drop} \geq t_{rad}$
 - Radiative limit at large d_d confirmed by μg experiments

- Large droplets not quasi-steady
 - Extinction occurs at sufficiently large d_d , but d_d decreases during burn - quasi-steady extinction not observable
 - K & d_f/d_d not constant - depend on d_{do} & time
 - Large time scale for diffusion of radiative products to far-field & O_2 from far-field
 - Soot accumulation dependent on d_{do}
 - Absorption of H_2O from products by fuel

Soot formation in μg droplet combustion

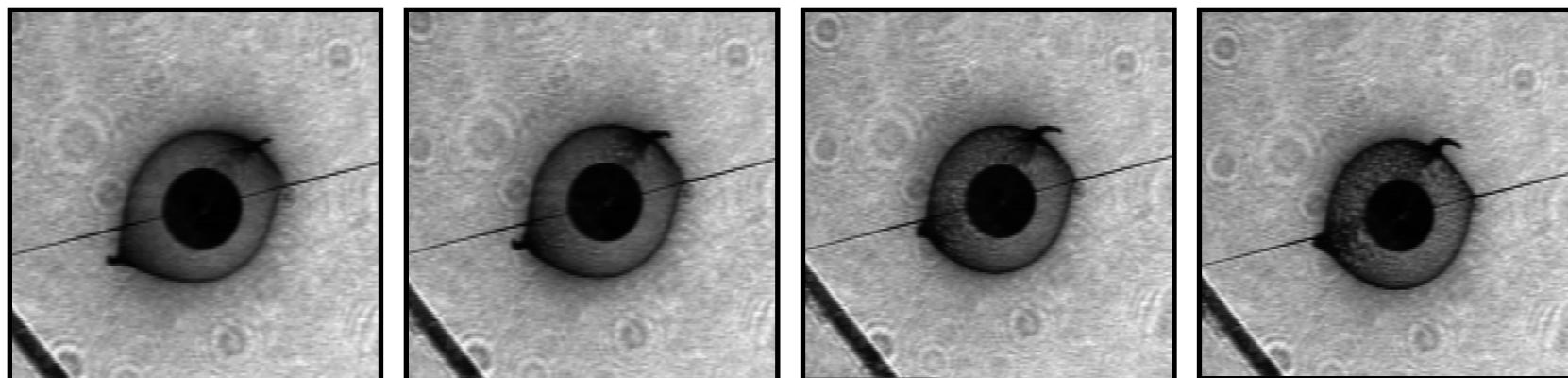


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0.5 sec

0.6 sec

0.7 sec

0.8 sec

n-heptane in air (Lee *et al.*, 1998)

➤ Radiative reabsorption effects

- Apparently seen in particle-seeded premixed-gas flames, flame balls, thin-fuel flame spread
- Easier to study at μg - no interference from turbulence
- Relevant to IC engines, large furnaces, EGR, flue-gas recirculation
- May occur in other μg flames, e.g.
 - » Droplet combustion - Stefan flow at surface limits conductive flux - $\ln(1+B)$ term; radiation not affected

$$\Omega = \ln\left(1 + \frac{B}{1 - R/\Omega}\right); R \equiv \frac{q_r d_d C_p}{2\lambda L_v}; \Omega \equiv \frac{K \rho_d C_p}{8\lambda}$$

» Flame spread over thick fuels - could lead to steady spread even at μg in O_2-CO_2 , O_2-SF_6

$$S_f = \left[\frac{\Lambda \alpha_g^2}{\sqrt{\alpha_g \rho_s C_{p,s} \lambda_s} (T_v - T_\infty) - \lambda_g (T_f - T_v)} \right]^{1/2}$$

➤ Need faster computational models of radiative transport!

- High-pressure combustion
 - Buoyancy effects ($t_{\text{chem}}/t_{\text{vis}}$) increase with P for weak mixtures
 - Reabsorption effects increase with P
 - Turbulence more problematic
 - Few μg studies - mostly droplets
- 3-d effects
 - Flame spread - effects of fuel bed width
 - Flame balls - breakup of balls
- Gas-jet flames at μg
 - Soot formation - what causes smoke points at μg ???
 - Slot jet vs. round-jet
 - Radiative extinction at large $d(0)$?

- Spherical diffusion flames - porous sphere experiment
 - Liquid or gaseous fuel
 - Could provide quasi-steady spherical nonpremixed flame
 - Increase fuel mass flow slowly until extinction
 - Difficult experimentally - long times, large chamber
 - Initial results with gaseous fuel - steady-state not reached - should use diluted fuel & enriched O_2 - increases f , reduces $d_f \Rightarrow$ smaller t_{drop}
- “Catalytic flame ball”
 - 1d, steady catalytic system
 - Radius known, T_* and Y_* unknown
 - Extract overall surface reaction rates

$$\Theta(Y_s, T_s) = \rho_s D_s r_s Y_\infty (1 - Y_s / Y_\infty) / M; \frac{Y_s}{Y_\infty} = 1 - Le \left(\frac{T_s - T_\infty}{T_{ad} - T_\infty} \right) \left(1 + \frac{\sigma \varepsilon_s r_s (T_s^4 - T_\infty^4)}{\lambda_s (T_s - T_\infty)} \right)$$

- Chemical models
 - Many μ g combustion phenomena of interest occur near extinction limits
 - Sensitive to chemical mechanism - branching vs. recombination
 - $H + O_2 + M \rightarrow HO_2 + M$ identified for further study
- Could Chaperon efficiency relative to N_2 be temperature dependent?

- Nonuniform flow, unsteady/curved flames: “flame stretch”

$$\Sigma \equiv \frac{1}{A} \frac{dA}{dt} \quad (\text{A} = \text{flame area})$$

- Strong stretch ($\Sigma^{-1} \approx t_{\text{chem}}$) extinguishes flames
- Moderate stretch strengthens flames for $\text{Le} < 1$

$$\text{Le} \equiv \frac{\text{Thermal diffusivity of the bulk mixture } (\alpha)}{\text{Mass diffusivity of scarce reactant into the bulk mixture } (D)}$$

- Spherical expanding flames, $\text{Le} < 1$: stretch allows flames to exist in mixtures below radiative limit until r_f too large & curvature benefit too weak

$$\Sigma \equiv \frac{1}{A} \frac{dA}{dt} = \frac{1}{4\pi r_f^2} \frac{d}{dt} (4\pi r_f^2) = \frac{2}{r_f} \frac{dr_f}{dt}$$

Dual limit: radiation at large r_f , curvature-induced stretch at small r_f (ignition limit)

- Counterflow configuration (Tohoku group)
 - $\Sigma = dU/dy$ – flame located where $U = S_L$
- Increased stretch pushes flame closer to stagnation plane
 - Decreased volume of radiant products
- Similar Le effects as curved flames
- Results
 - Dual limits
 - Flammability extension even for $Le > 1$
 - Multiple solutions (which ones are stable?)
- Dual limits & Le effects seen in μg experiments, but evidence for multivalued behavior inconclusive